

SULPHIDE MODELLING IN ICM TO IDENTIFY CORROSION POTENTIAL

Manu Ward
Rebecca Buchanan



Presentation outline

1. The problem
2. The science
3. The tool - ICM
4. Trial results (Hutt Valley)
5. Validation checks
6. Conclusions





Figure 4 Cavity as first observed, 6 December 2019

Source: Ian Martin, AECOM (2020) report



Figure 7 Screengrab from Hydrotech camera footage

Kiwi Street, 2013



Kiwi Street, 2013



Kiwi Street, 2013



Kiwi Street, 2013



Kiwi Street, 2013



Kiwi Street, 2013



Kiwi Street, 2013



Kiwi Street, 2013



Kiwi Street, 2013



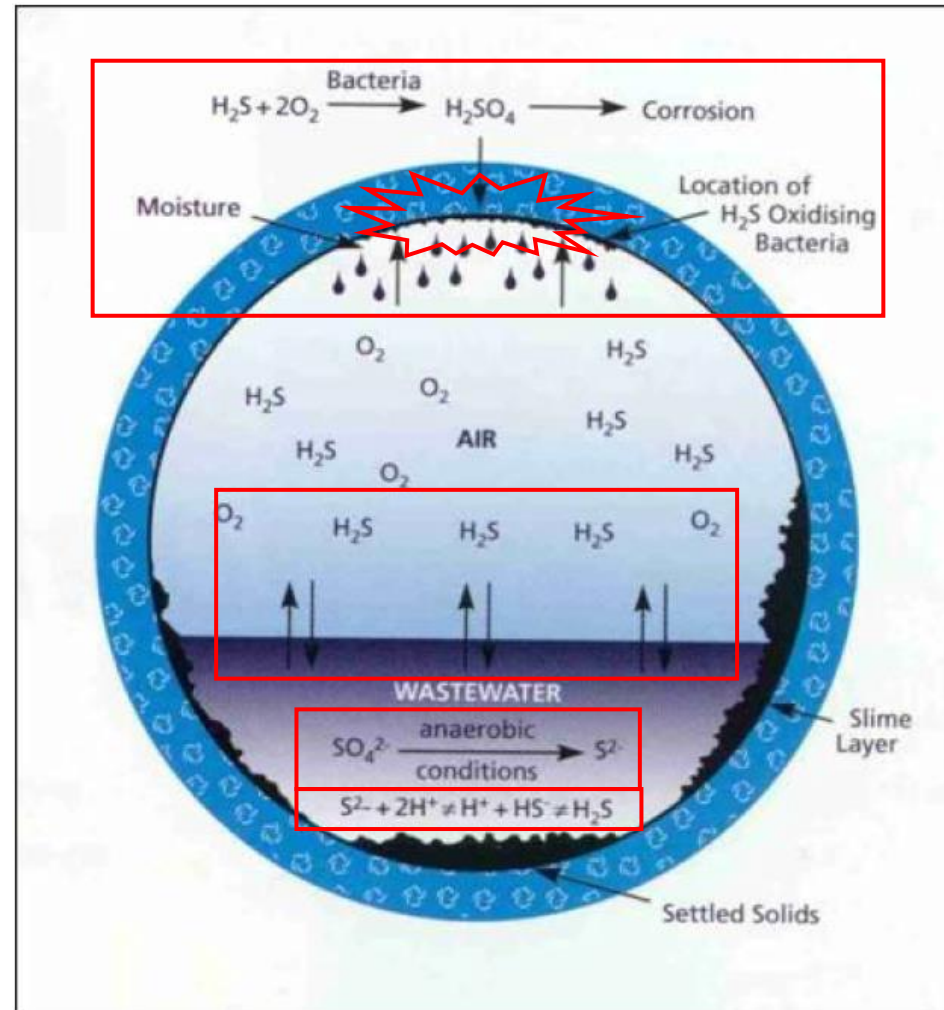
Source: Steve Hutchison, Wellington Water

The problem

1. Sulphide is characterised by “sporadic” or “seemingly random” appearance (until processes are better understood)
2. Corrosion can be gradual and undetected
3. Can seriously impact asset lifespan – to as little as 3 years
4. Historically addressed reactively
5. High cost of emergency maintenance or renewal
6. Odour and toxicity of gaseous sulphide

The science

1. Sulphates to sulphides (septic conditions)
2. Total sulphides to dissolved H_2S
3. Dissolved to gaseous H_2S
4. Oxidised by bacteria to H_2SO_4 in condensation
5. Acid attacks concrete, iron, steel (but not clay or plastic)



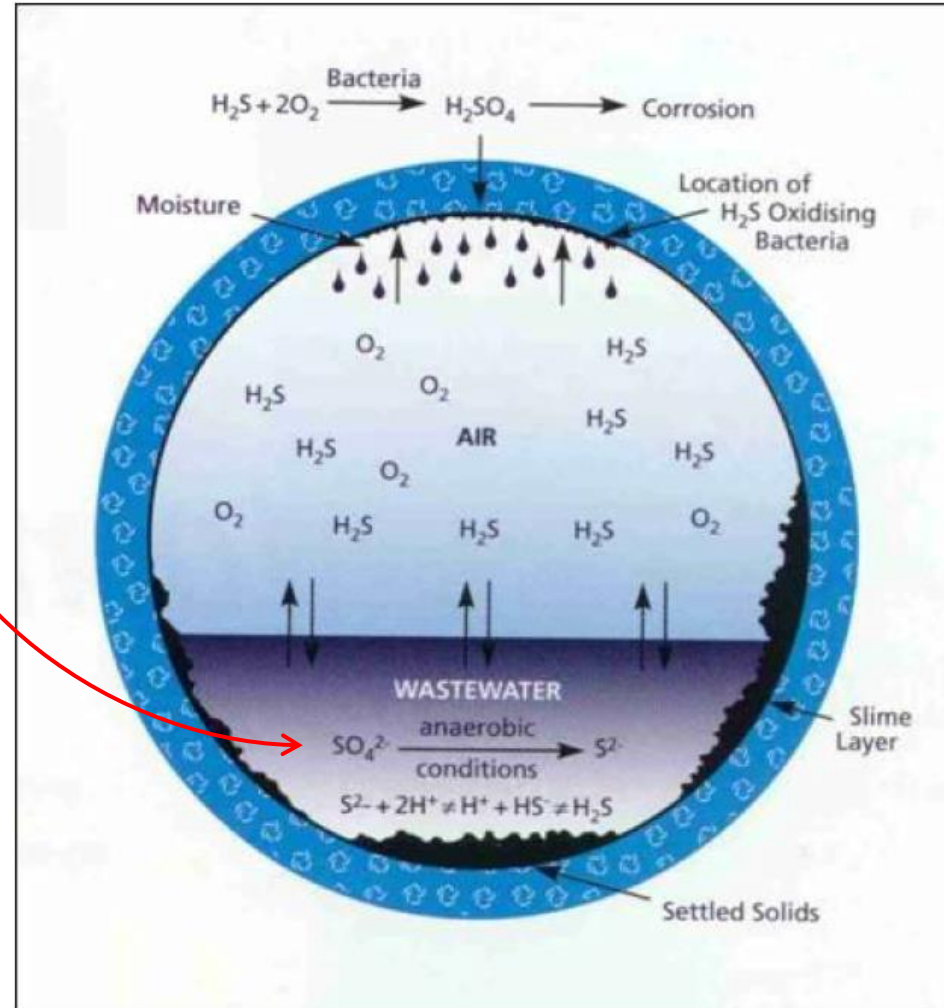
The basic process of sulphide release in a septic environment (Cisca & Crosby, 2015)

The tool

Pomeroy's Equation

$$\frac{d[S]}{dt} = \frac{M' EBOD}{R} - \frac{m[S](su)^{\frac{3}{8}}}{d_m}$$

M'	Sulphide flux free coefficient (Default = 0.00032 m/h)
$EBOD$	$BOD \times 1.07^{(T-20)}$
T	Wastewater temperature (°C)
R	Hydraulic Radius (m)
m	Sulphide loss coefficient – empirical coefficient accounts for losses by oxidation and escape to atmosphere (Default = 0.64 (m/h) $_{(m/s)^{-3/8}}$)
$[S]$	Total sulphide concentration (mg/L)
d_m	Mean hydraulic depth (m)
u	Mean sewerage velocity (m/s)
s	Slope of energy grade line (m/m)



The basic process of sulphide release in a septic environment (Cisca & Crosby, 2015)

The tool

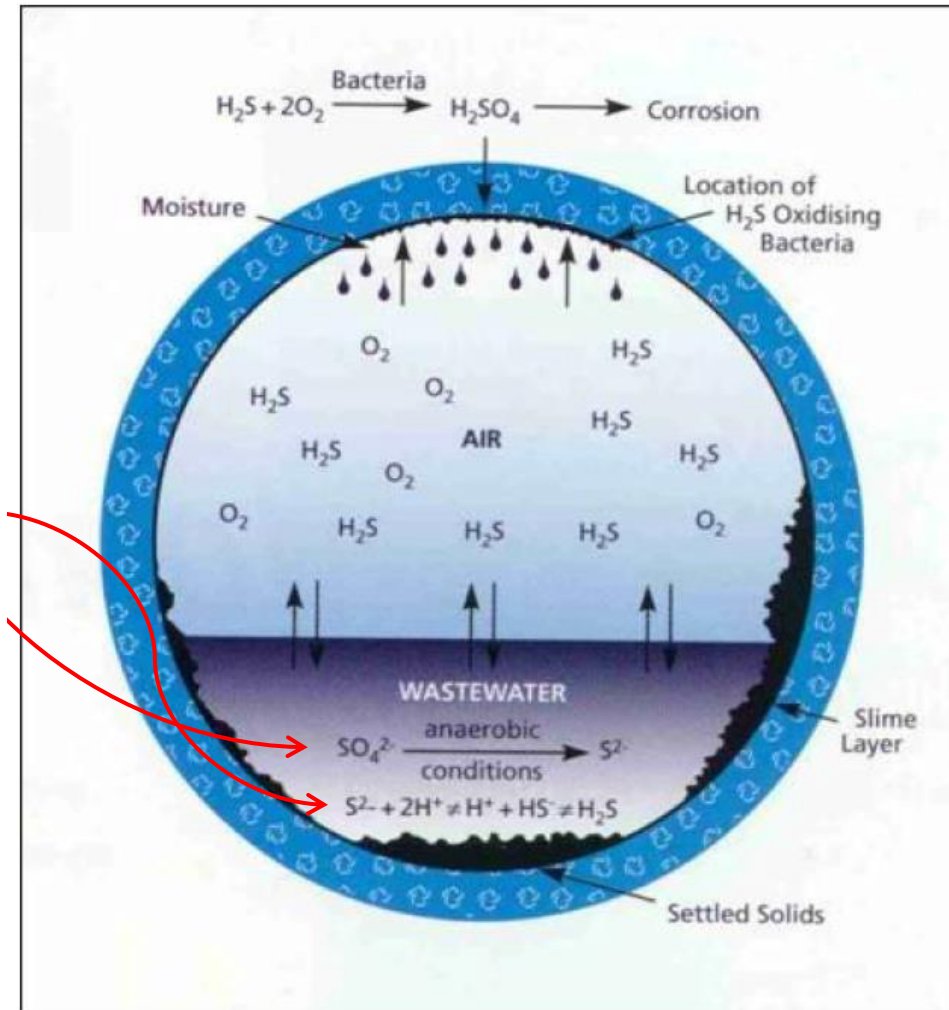
Pomeroy's Equation

$$\frac{d[S]}{dt} = \frac{M' EBOD}{R} - \frac{m[S](su)^{\frac{3}{8}}}{d_m}$$

Sulphide solubility

$$H_2S = \frac{\% \text{ soluble sulphide}}{100} \times 1.0625 \times \frac{1}{1 + \frac{10^{-pK_1}}{10^{-pH}}} \times \text{Total Sulphide}$$

pK_1	Ionisation coefficient (default = 7.0)
1.0625	H_2S and S^{2-} molecular weight ratio
% Soluble Sulphide	(Default = 80%)



The basic process of sulphide release in a septic environment (Cisca & Crosby, 2015)

QM Parameters

Select Pollutants and Sediment Fractions to Model

	Dissolved	SF1	SF2
Model	<input checked="" type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
BOD	<input checked="" type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
COD	<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
TKN	<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
NH4	<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
TPH	<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
PL1	<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
PL2	<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
PL3	<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
PL4	<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
DO	<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
NO2	<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
NO3	<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
PH	<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
SAL	<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
TW	<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
COL	<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
ALG	<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
SI	<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>

- ☐ Dependent sediment fractions
- ☒ Erosion/deposition affects hydraulics
- ☐ Override event buildup time
- ☐ Model macrophytes
- ☒ Model hydrogen sulphide
- ☐ Model 2D erosion-deposition
- ☐ Model 2D bed load

QM multiplier (0 means use minor time-step)

Buildup time (hours)

Oxygen demand

☒ Native washoff routing

OK

Cancel

Export To...

Run simulations

Simulation providing initial state:

Sim >> X

- ☐ Always use state without re-initialisation
- ☐ Start running from state time

Initial conditions 1D/2D >> X

Catchment initial conditions >> X

Do not save state 00:00 00/00/0000

☐ Simulate runoff only: Whole run

Warm-up duration: Minutes 0

- ☒ Apply rainfall smoothing
- ☒ Summary (PRN) results
- ☐ Exit if initialisation incomplete in (mins): 1000
- ☒ Exit if initialisation fails
- ☒ Initialise by level fill-in from outfalls
- ☒ Use QM

Pipe sediment data >> X

QM parameters

2D parameters

timestep control

Diagnostics

Description 2 FG02_Residential

Edit...

Add...

Delete

(Profile = 2)

Flow

Per Capita Flow (l/day) 124.697

Sediment

Sediment fraction 1 (mg/l) 0.000

Timesteps

Calibration profiles: 01:00

Change...

Design profiles: 01:00

Change...

Pollutant

Dissolved

Pollutant	Concentration (mg/l)
BOD	199.000
COD	507.000
TKN	35.000
NH4	20.000
TPH	5.600
PL1	0.000
PL2	0.000
PL3	0.000
PL4	0.000
DO	11.000
NO3	25.000
NO2	0.100

PH 7.500

SAL (kg/m3) 95.000

TW (degC) 20.000

COL 20000.000

Title User defined WWG item

Run simulations

Simulation providing initial state:

Sim

☐ Always use state without re-initialisation☐ Start running from state time

Initial conditions 1D/2D

Catchment initial conditions

Do not save state

00:00

00/00/0000

☐ Simulate runoff only:

Whole run

Warm-up duration:

Minutes

0

☒ Apply rainfall smoothing☒ Summary (PRN) results☐ Exit if initialisation incomplete in (mins):

1000

☒ Exit if initialisation fails☒ Initialise by level fill-in from outfalls☒ Use QM

Pipe sediment data

QM parameters

2D parameters

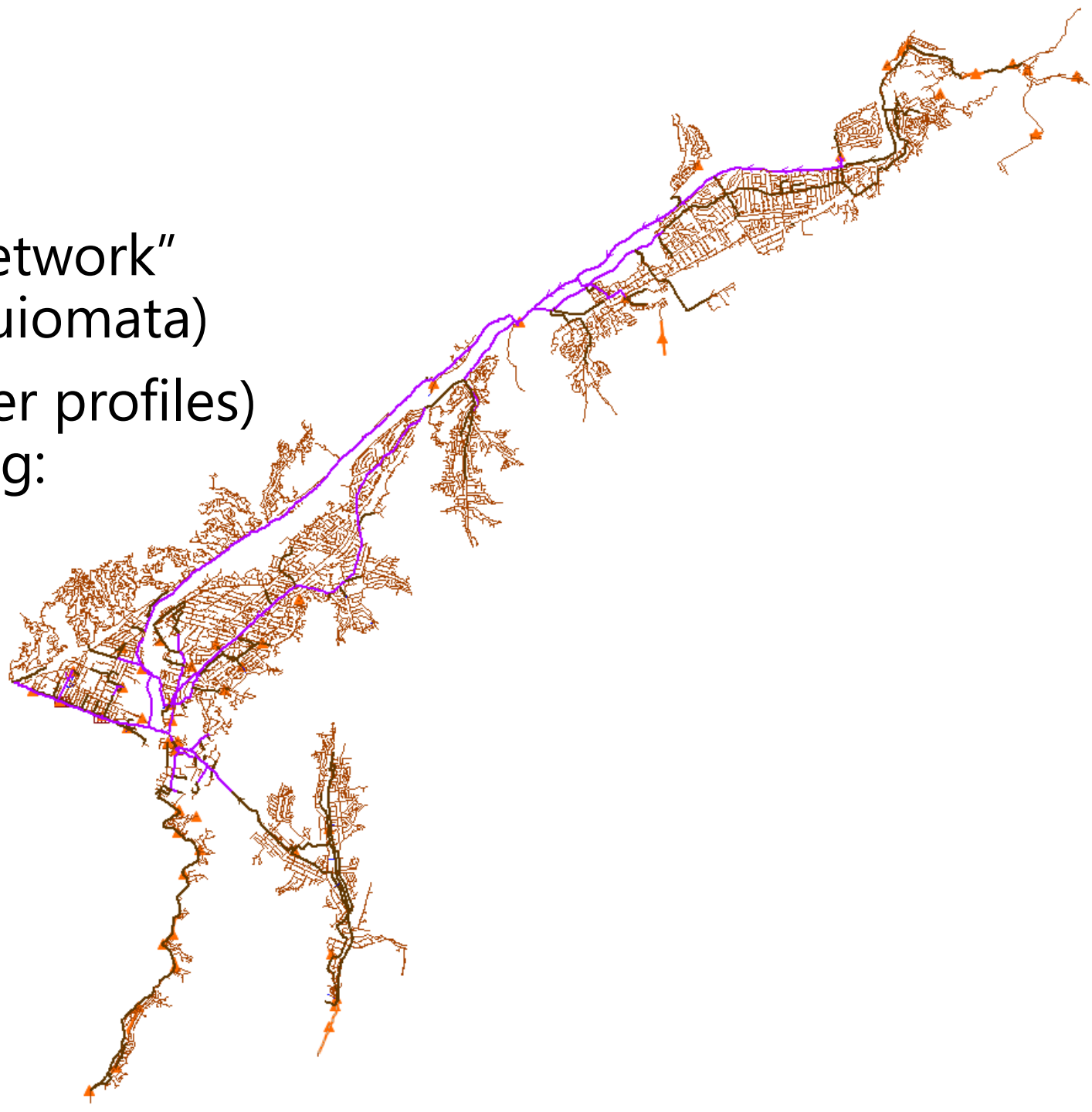
Timestep control

Diagnostics

Trial case – Hutt Valley





- All-pipes model of “Seaview Network” (Upper Hutt, Lower Hutt, Wainuiomata)
- Pollutant loading (all wastewater profiles) assumed for wastewater loading:

POLLUTANT	VALUE	MODELLED
pH	7.0	<input type="checkbox"/>
SAL (kg/m ³)	95	<input type="checkbox"/>
TW (degC)	20	<input type="checkbox"/>
COL	20,000	<input type="checkbox"/>
POLLUTANT	CONCENTRATION (MG/L)	MODELLED
BOD	199	<input checked="" type="checkbox"/>
COD	507	<input type="checkbox"/>
TKN	35	<input type="checkbox"/>
NH ₄	20	<input type="checkbox"/>
TPH	5.6	<input type="checkbox"/>
DO	11	<input type="checkbox"/>
NO ₃	25	<input type="checkbox"/>
NO ₂	0.1	<input type="checkbox"/>



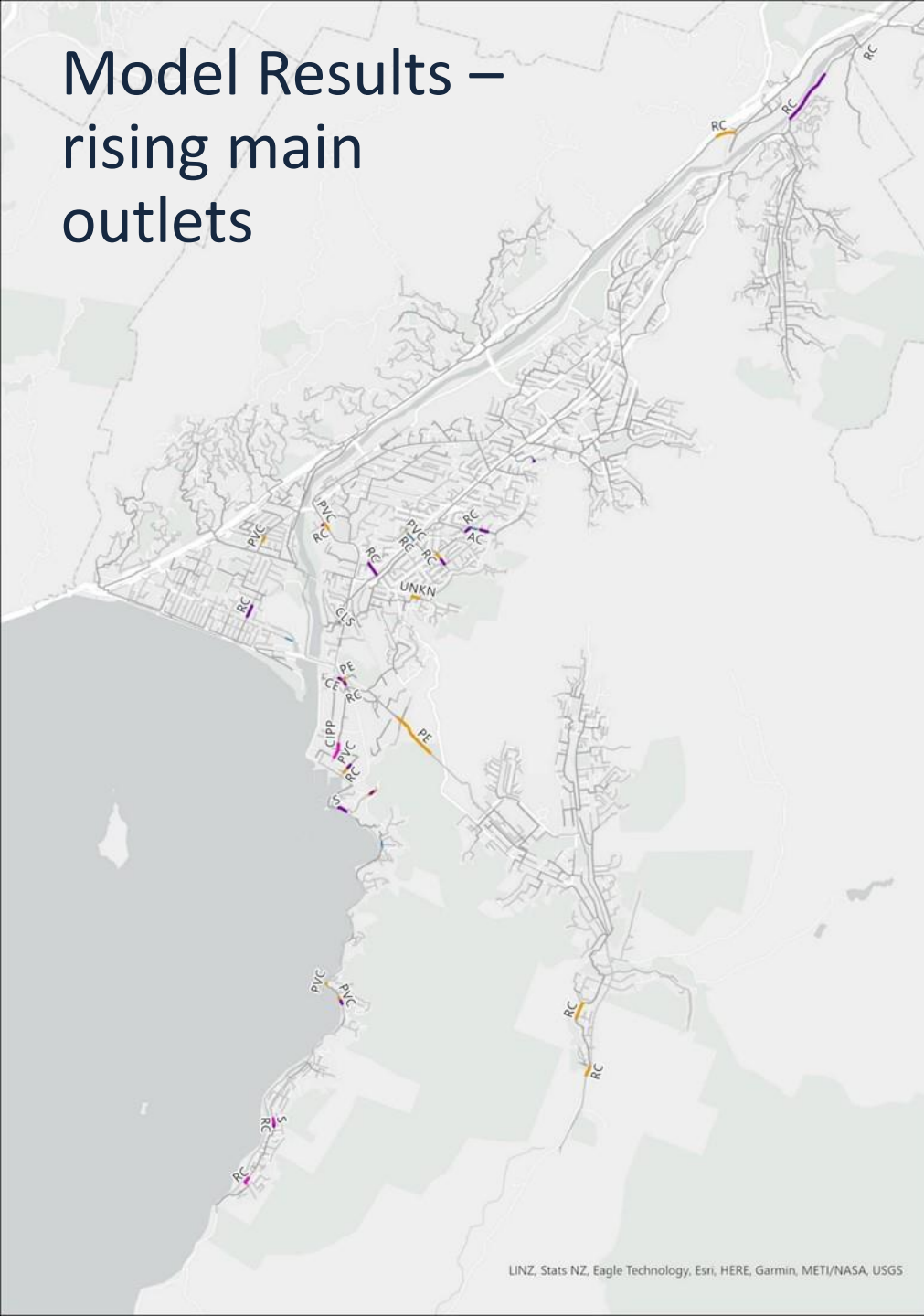
Model Results – Trunk Network

- Highlighting results for trunk network only
- 90th %ile of DWF 24-hr period
- Note Sydney Water targets <0.5 mg/L (blue lines)

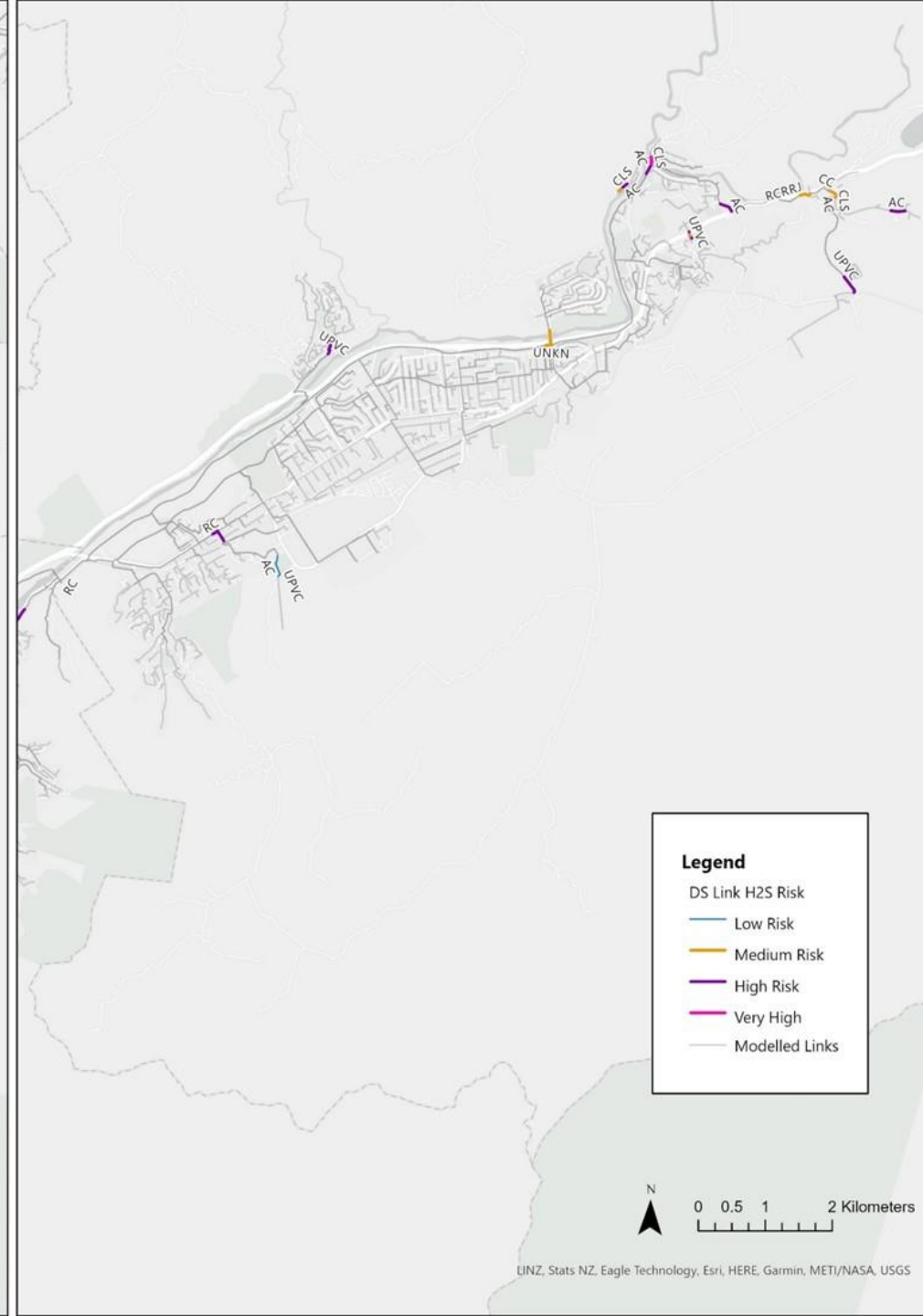
SYMBOLGY	DISSOLVED H ₂ S	CORROSION RISK
	< 0.5 mg/L	Low Risk
	0.5 – 1 mg/L	Medium Risk
	1 – 5 mg/L	High Risk
	>5 mg/L	Very High Risk



Model Results – rising main outlets



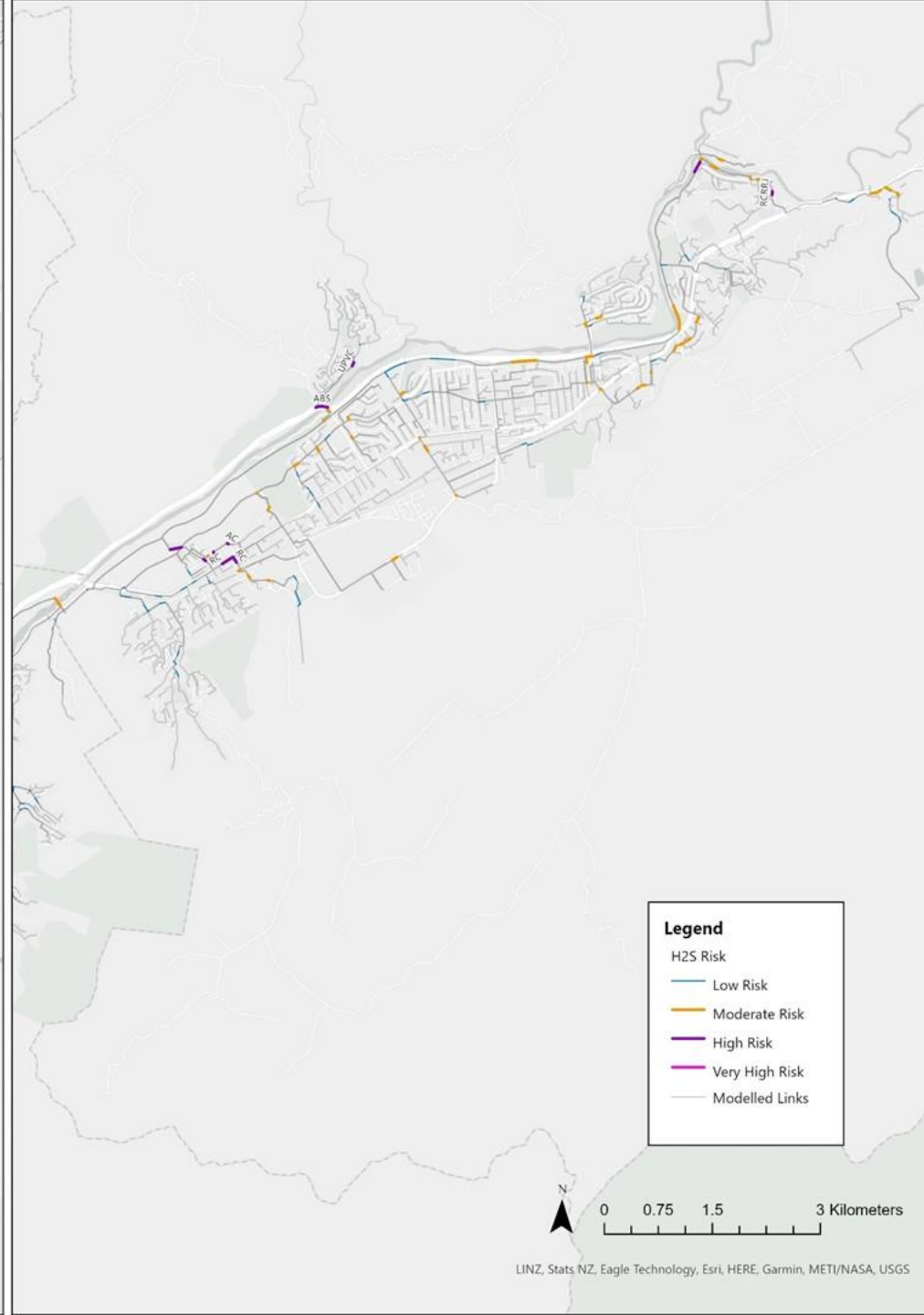
LINZ, Stats NZ, Eagle Technology, Esri, HERE, Garmin, METI/NASA, USGS



LINZ, Stats NZ, Eagle Technology, Esri, HERE, Garmin, METI/NASA, USGS

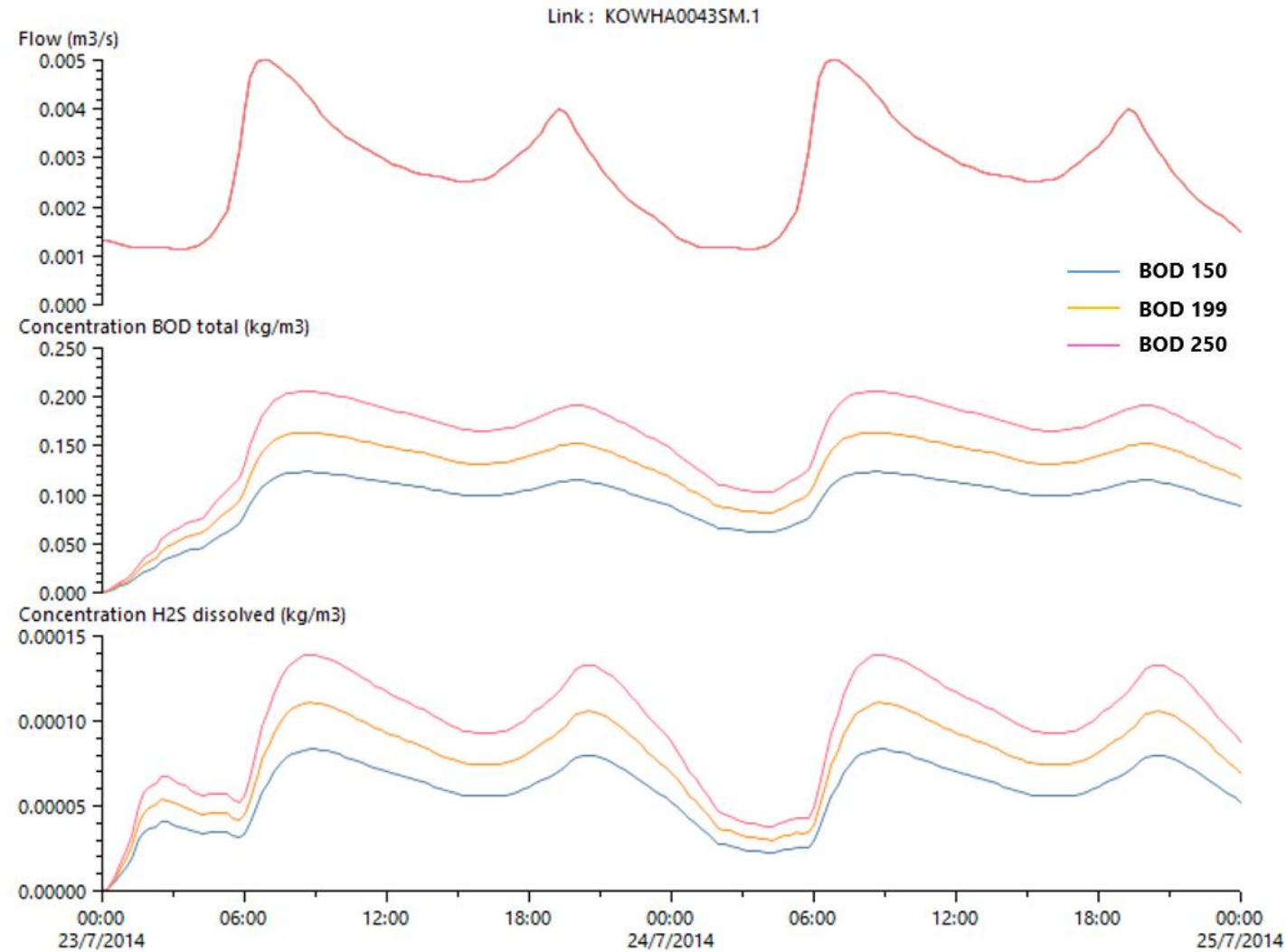
- Gravity mains downstream of a rising main
- 20 locations with >1 mg/L dissolved sulphide

Model Results – Hydraulic jump locations

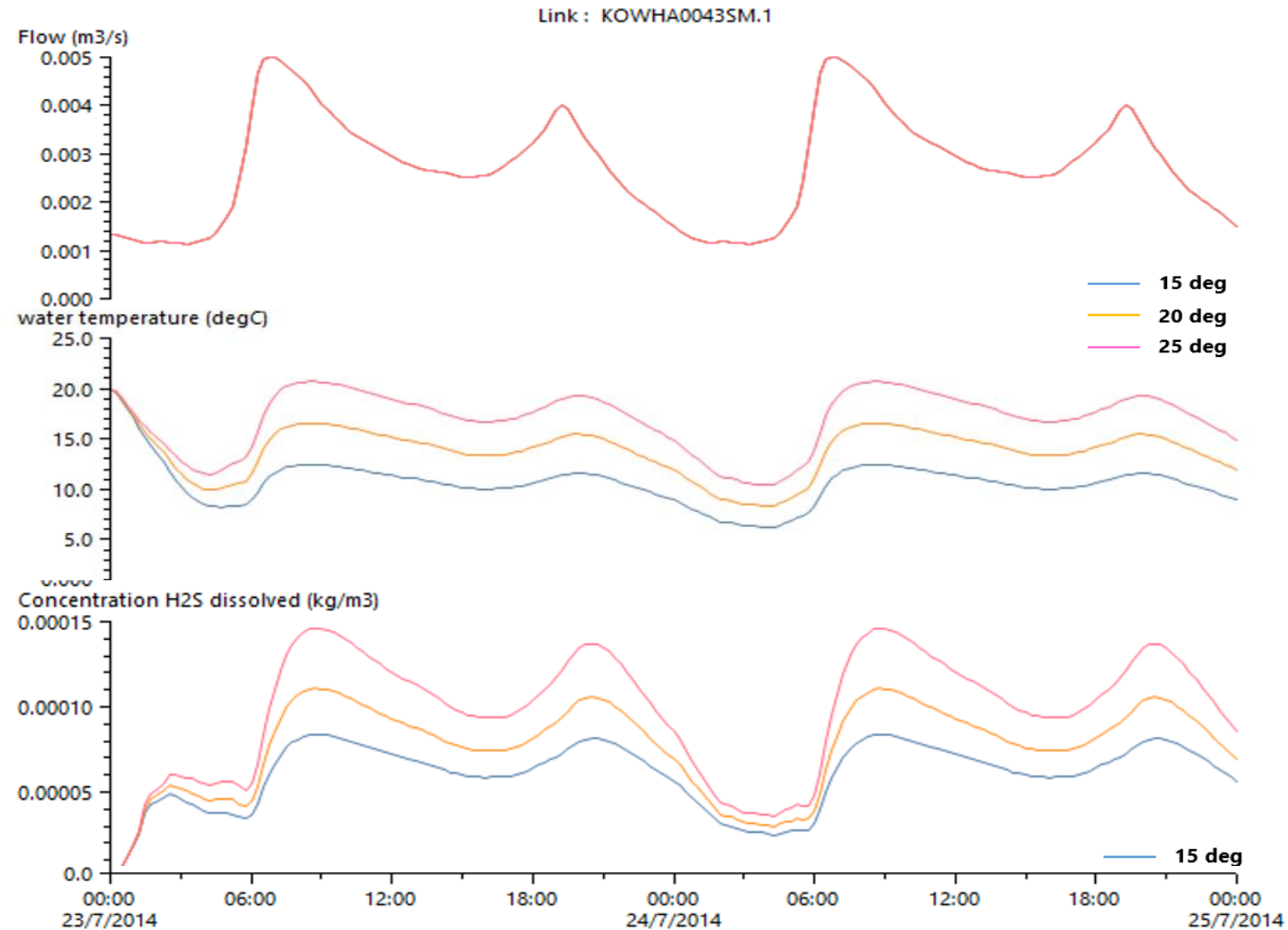


- Gravity pipes where max modelled Froude No. transitions from >1 to <1
- 25 locations with >1 mg/L dissolved sulphide

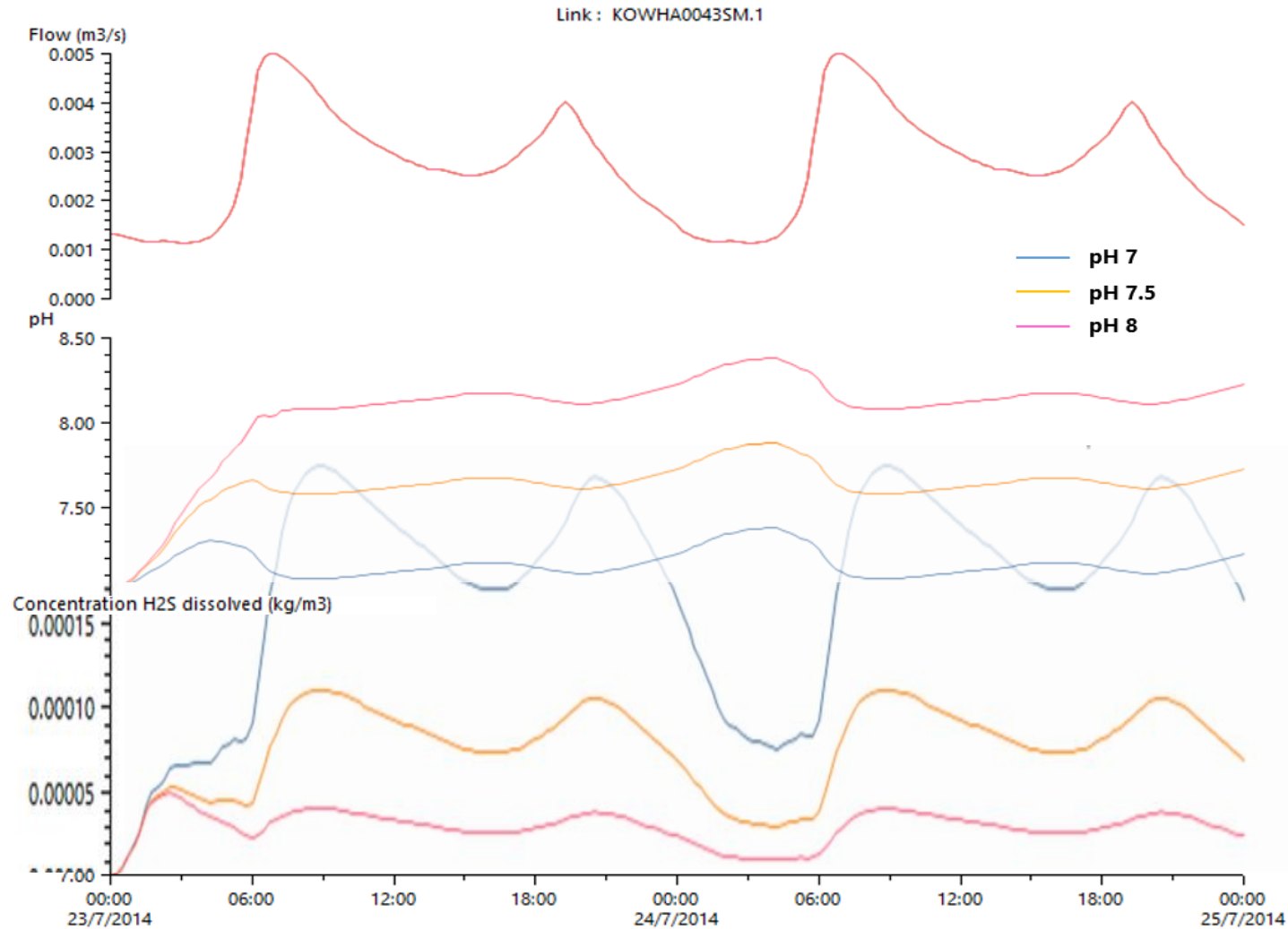
Results Sensitivity - BOD



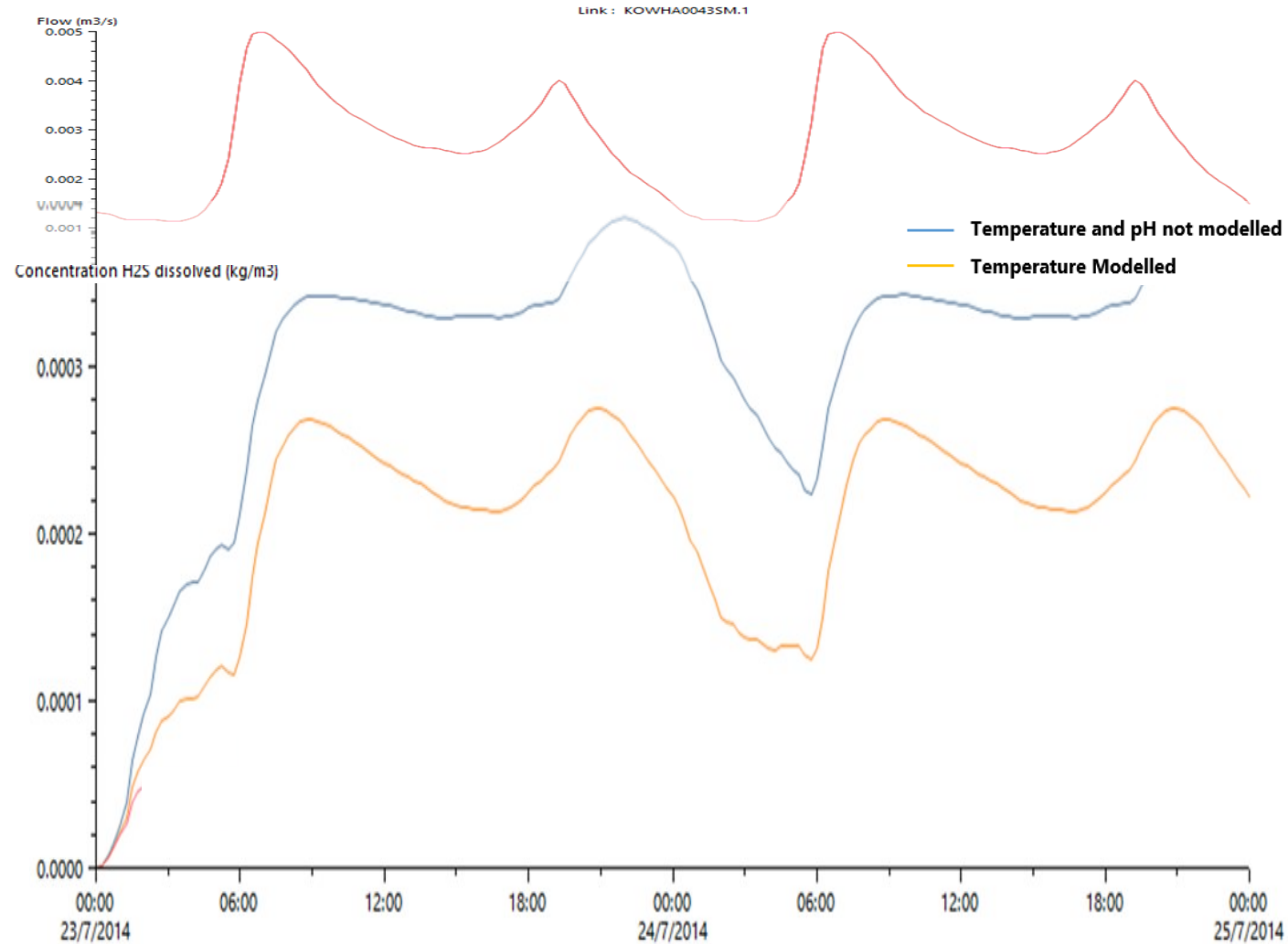
Results Sensitivity - Temperature



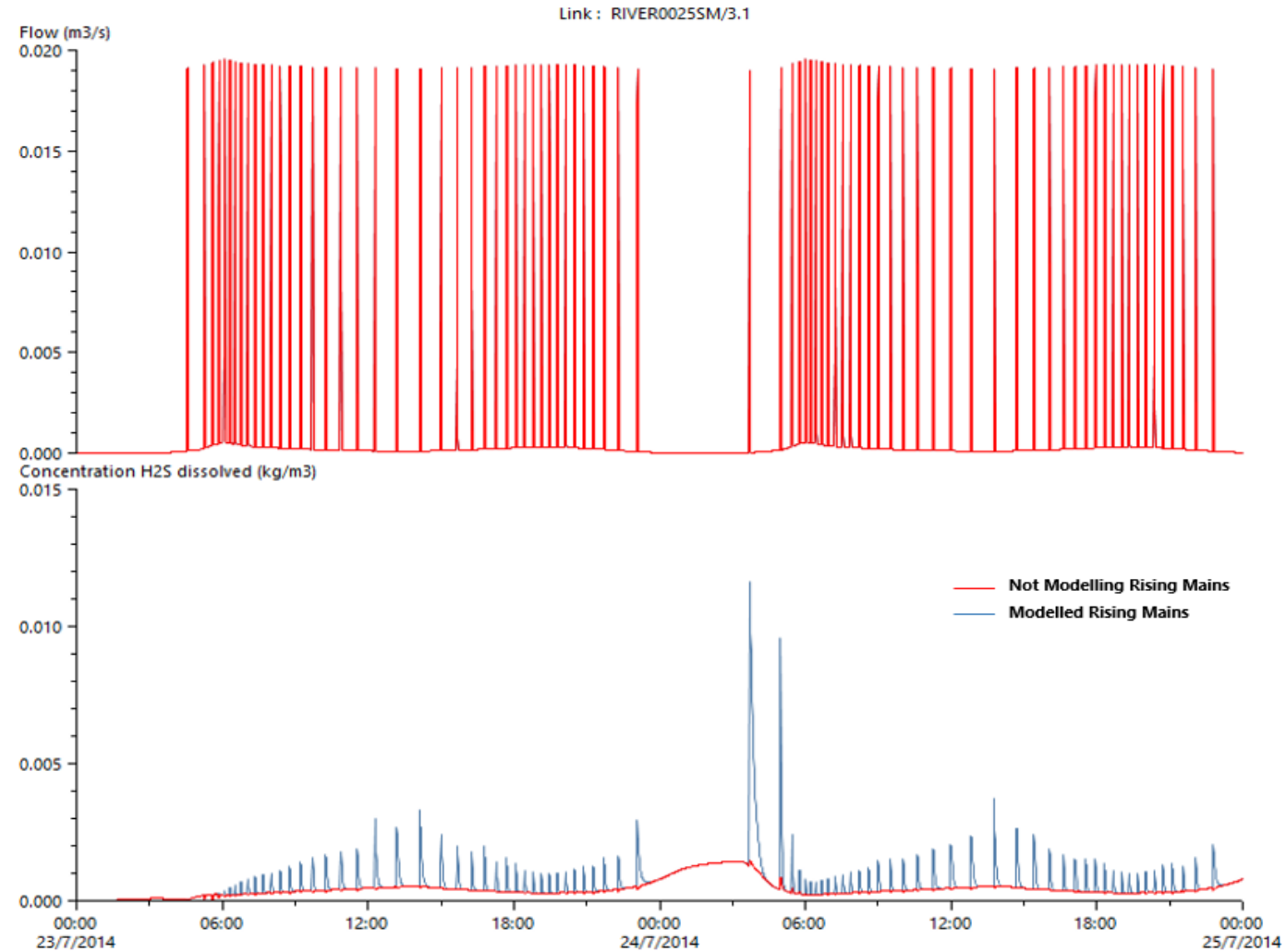
Results Sensitivity - pH



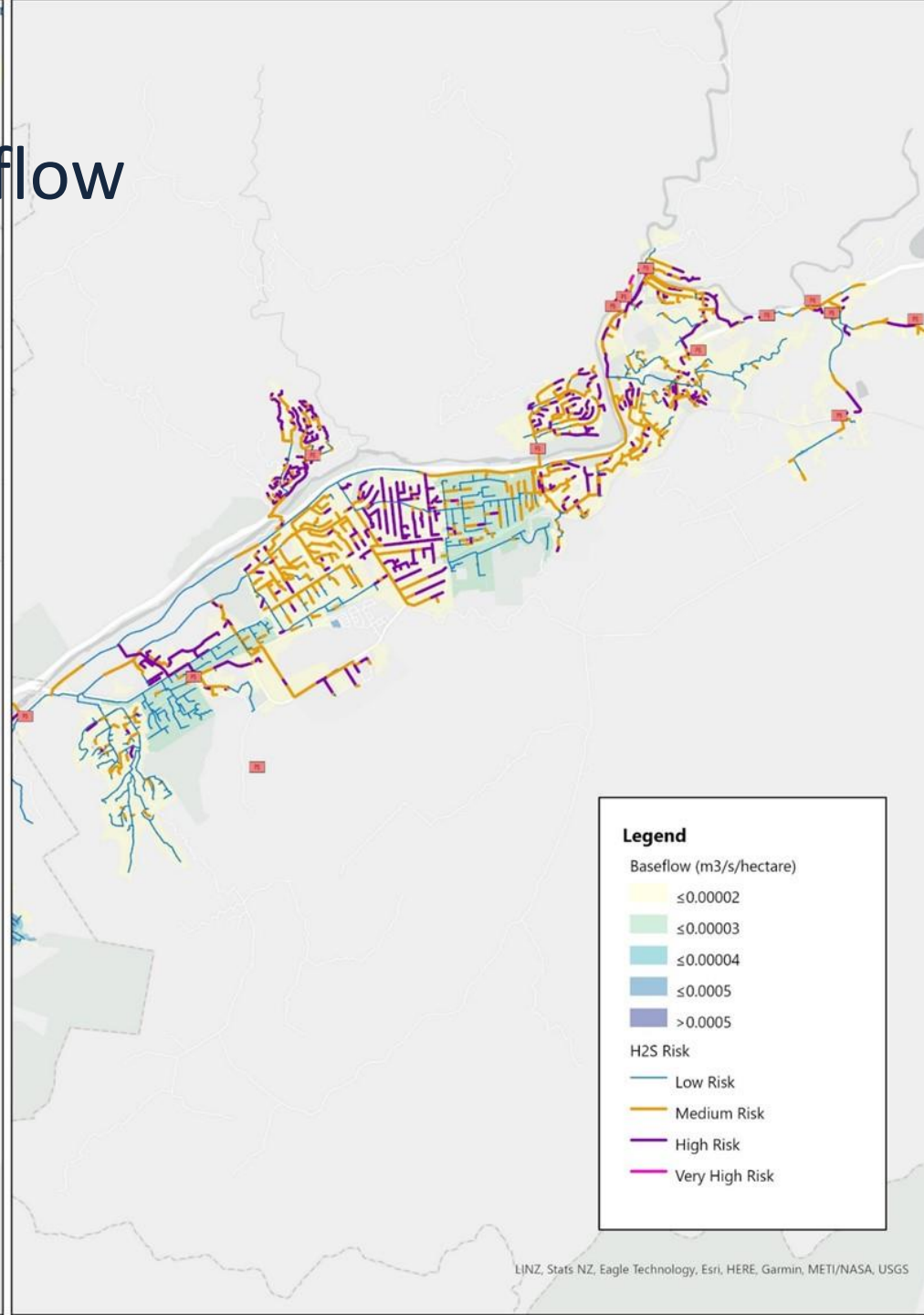
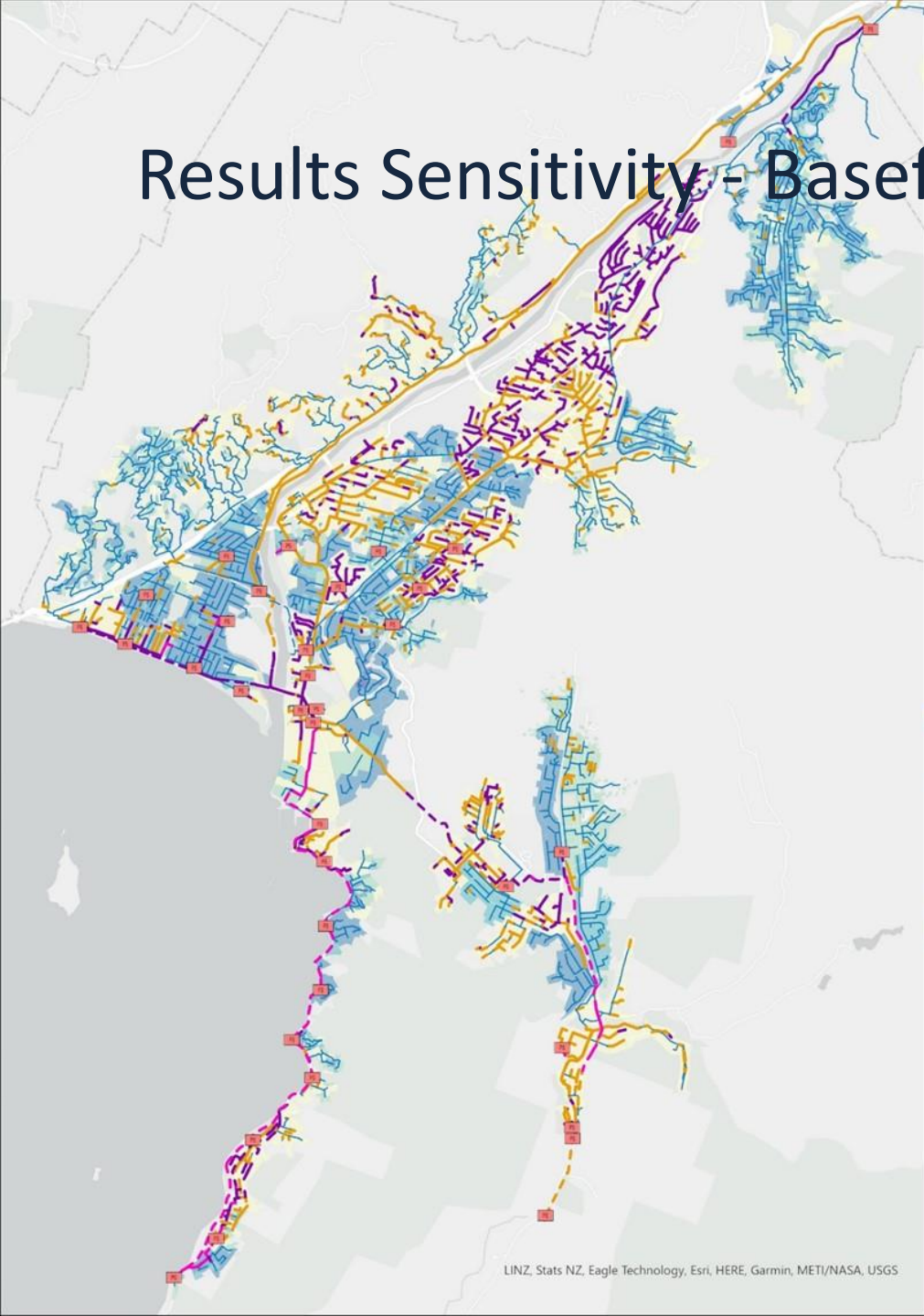
Results Sensitivity – WQ setup



Results Sensitivity - BOD



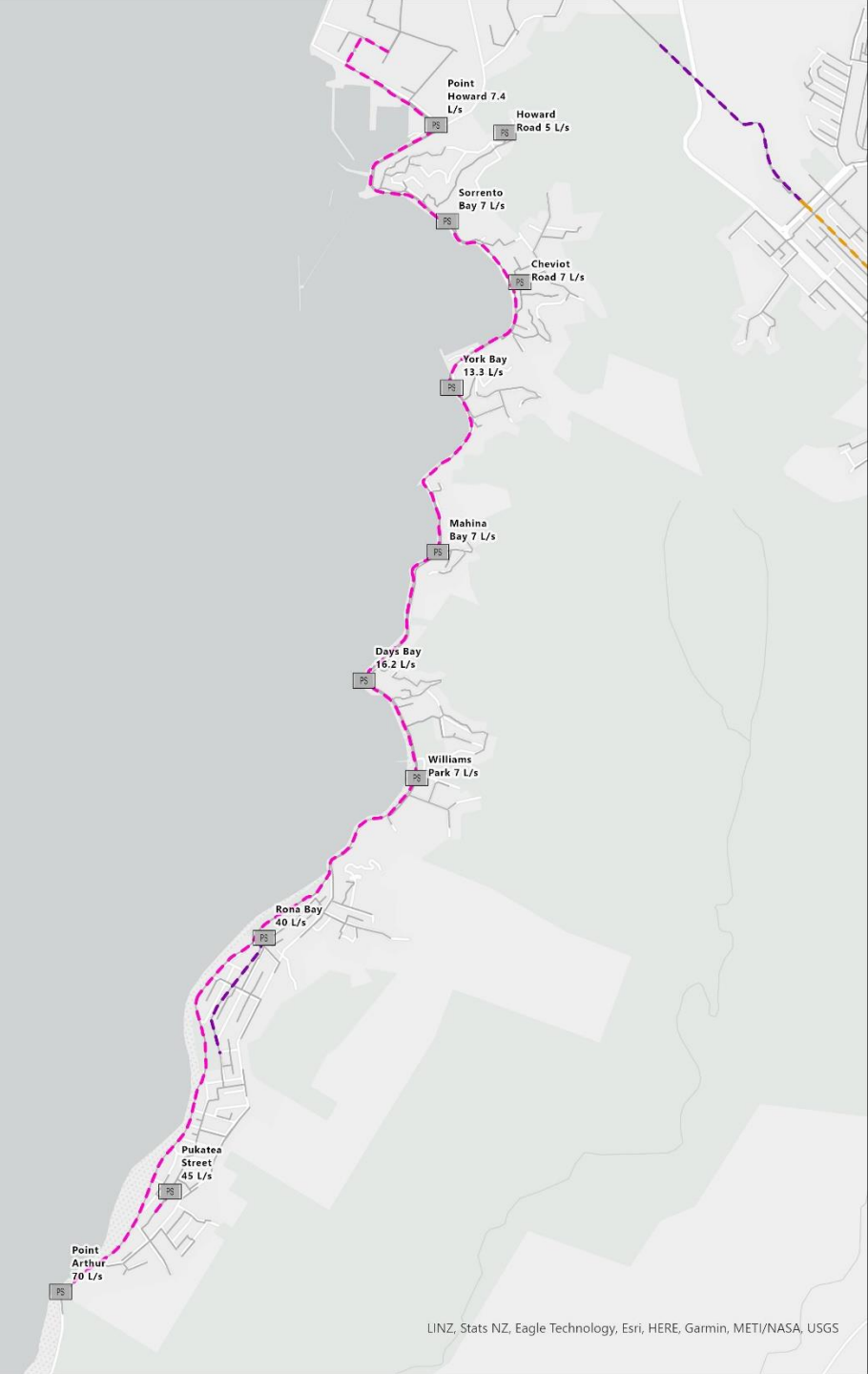
Results Sensitivity - Baseflow



- Baseflow reduces dissolved sulphide

Model validation – Pt Arthur

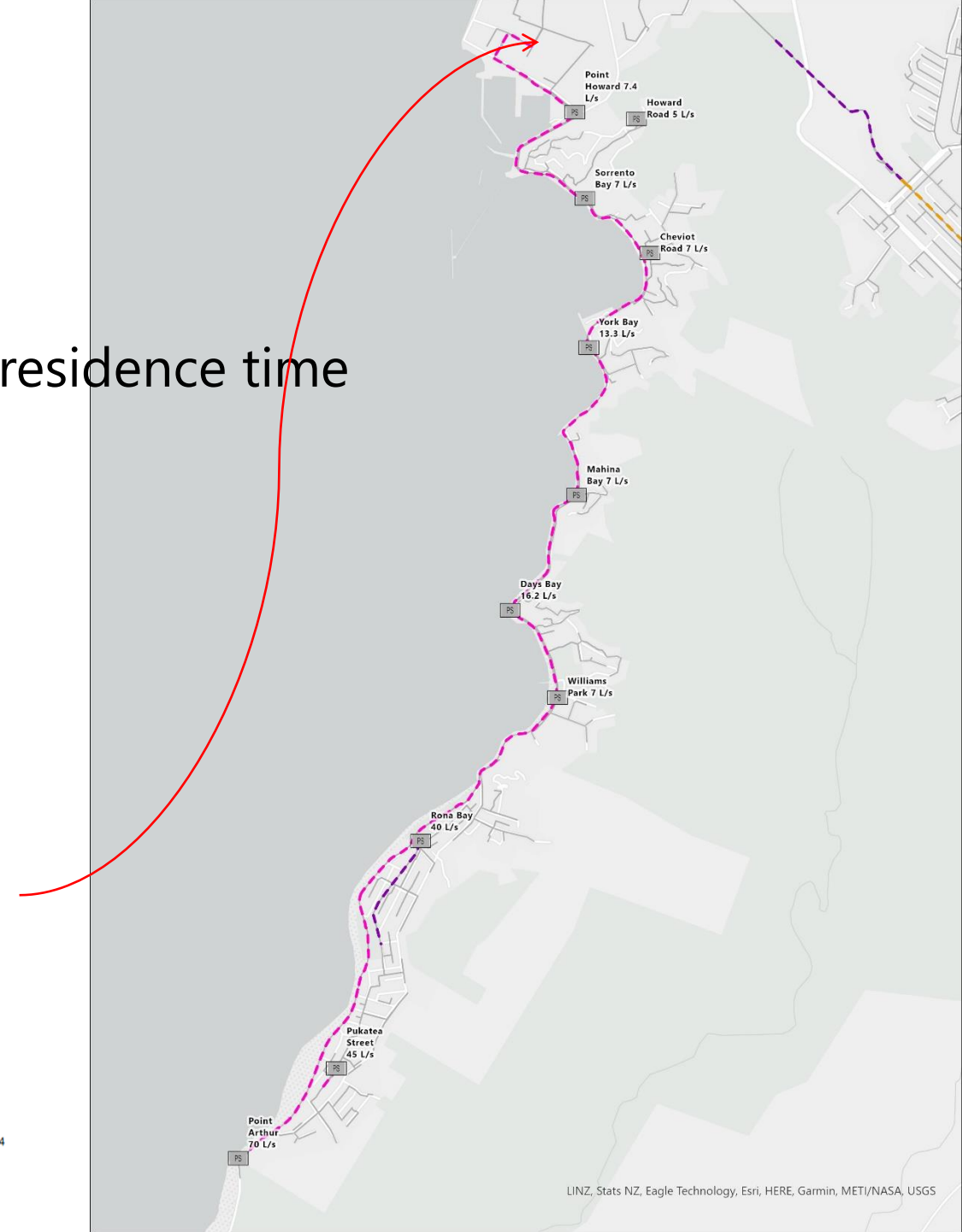
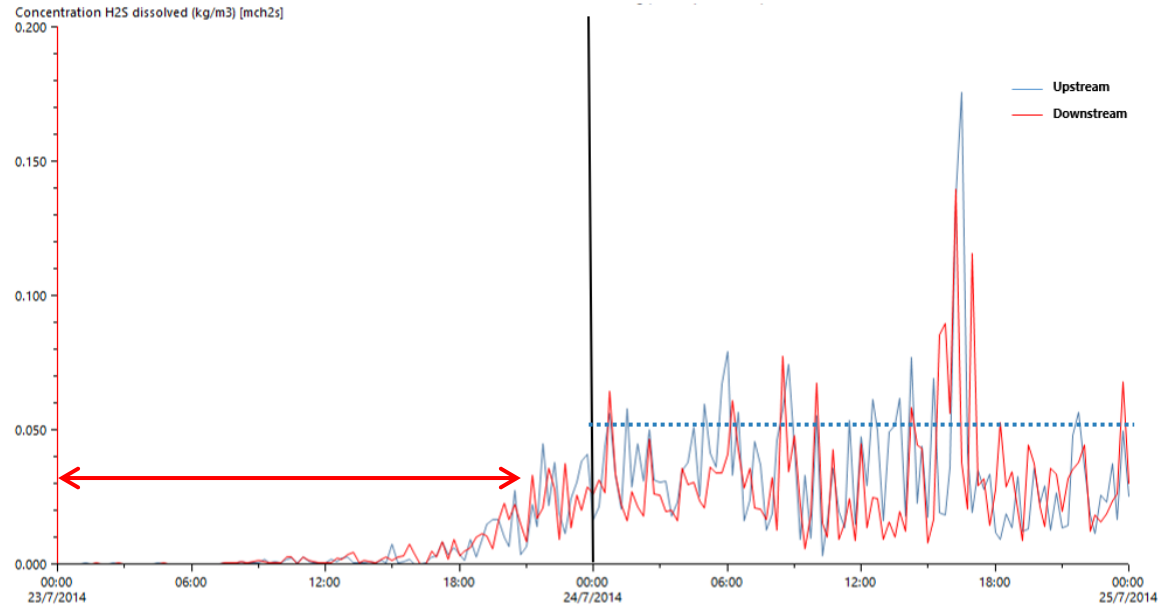
- 300 mm diameter rising main, 9.3 km,
- Pt Arthur catchment:
 - Population ~3,000
 - ADWF ~9 L/s
- Manual calculation:
 - Estimated residence time = 20.6 hrs
 - Dissolved sulphide at RM outlet = 26 mg/L



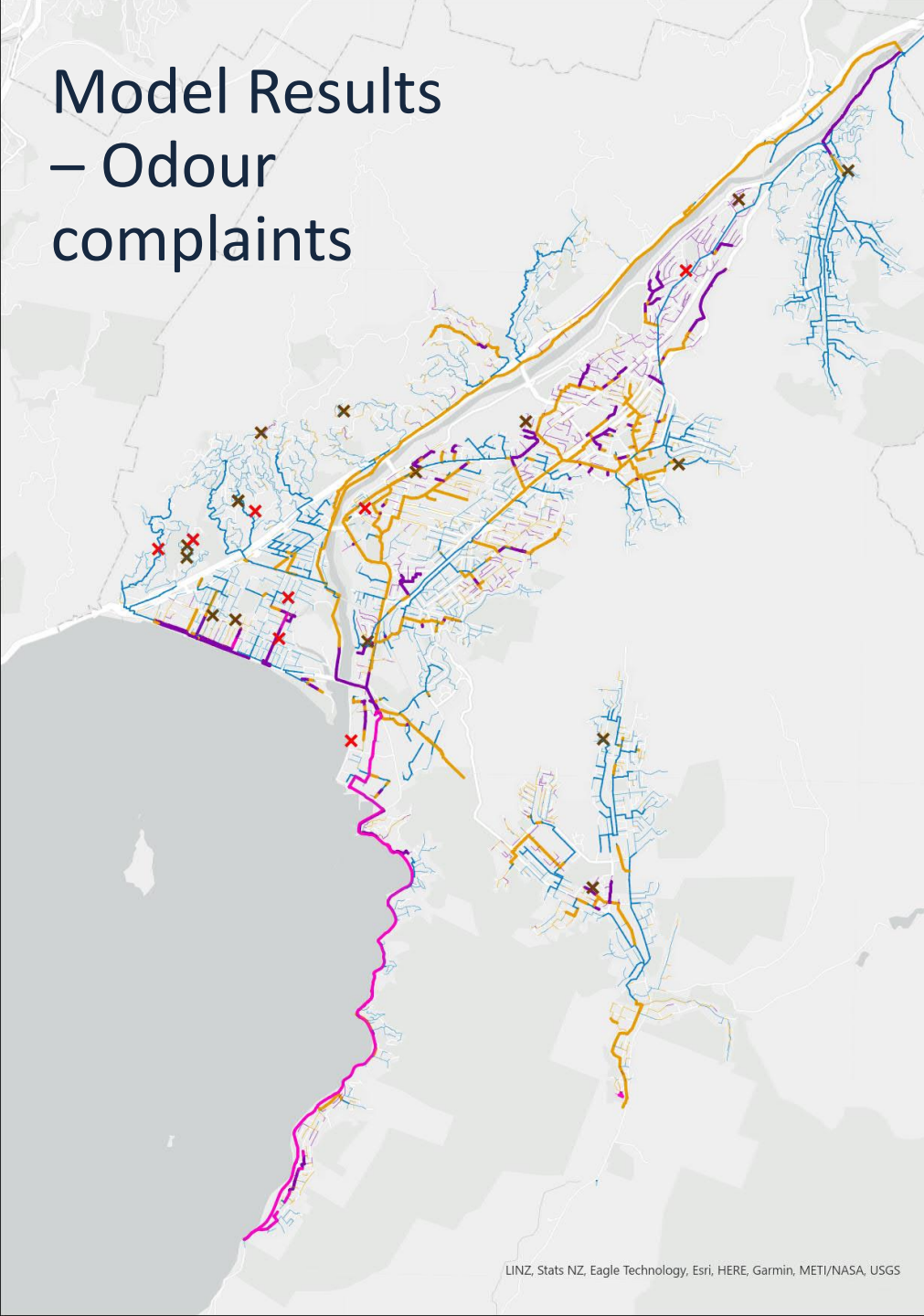
Model validation – Pt Arthur

- Modelled result:

- Build-up time corresponds to estimated residence time
- Average dissolved sulphide = 51 mg/L

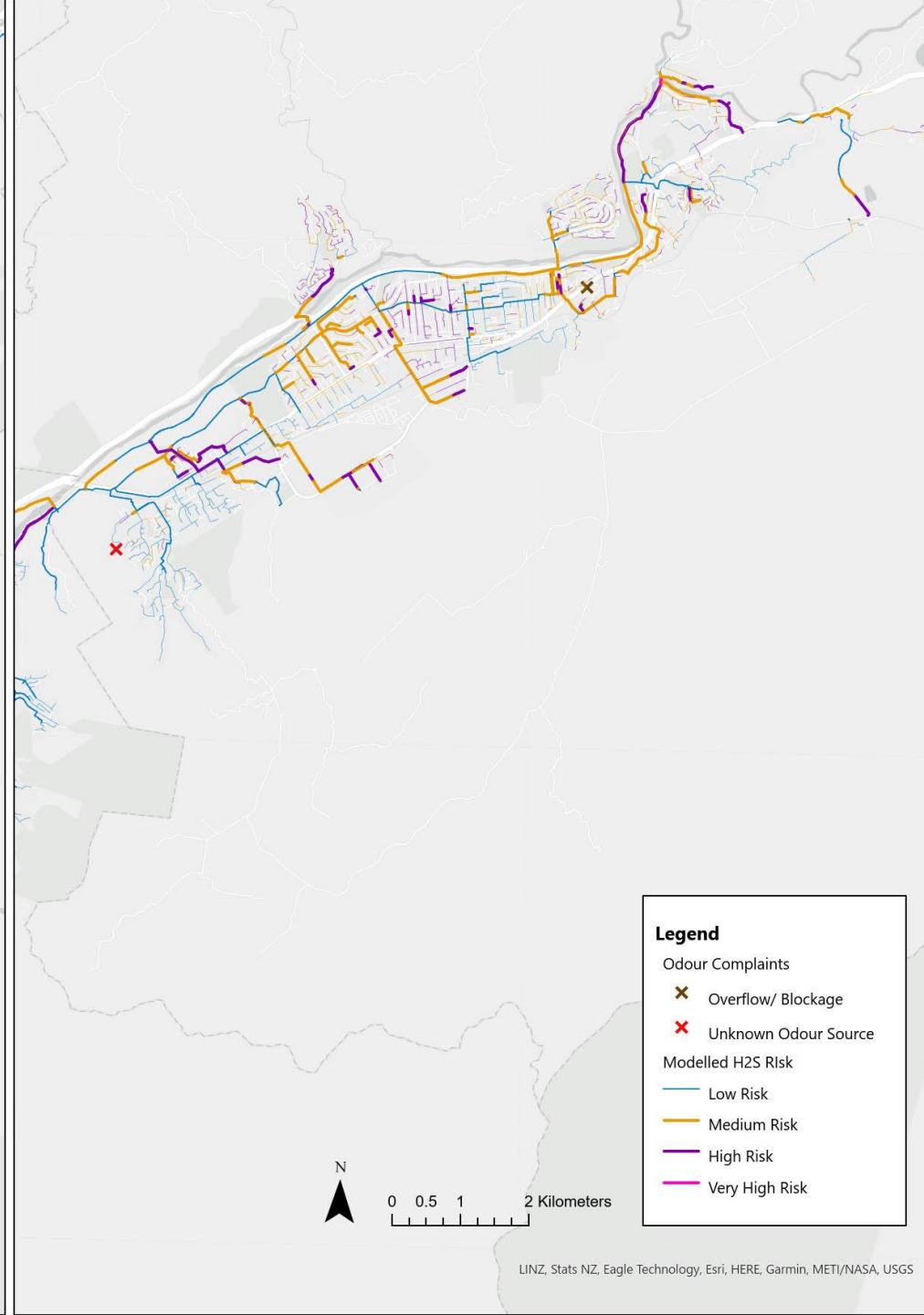


Model Results – Odour complaints



LINZ, Stats NZ, Eagle Technology, Esri, HERE, Garmin, METI/NASA, USGS

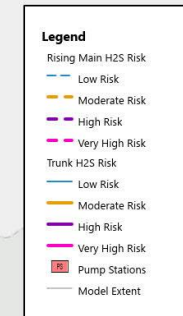
- Filtered customer complaints



Model Results – Past failures

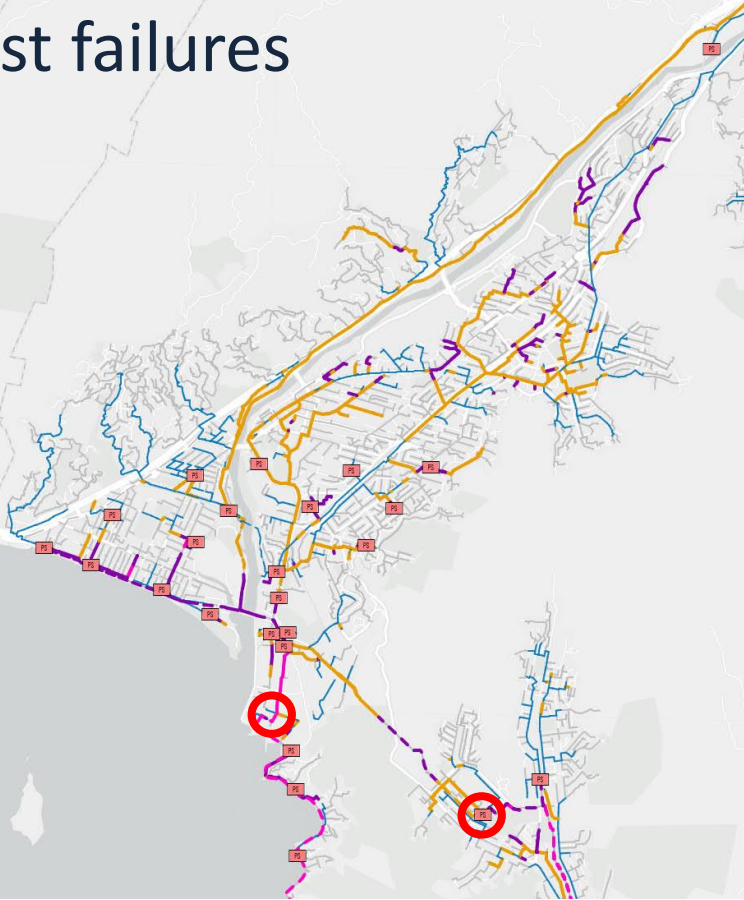
- Operational knowledge

- Collapsed - 2001 (6 years after Pt Arthur RM installed).
- >300m pipe replaced with PVC, HDPE, or CIPP.
- Pumps upgraded to ensure flushing.



0 0.5 1 2 Kilometers

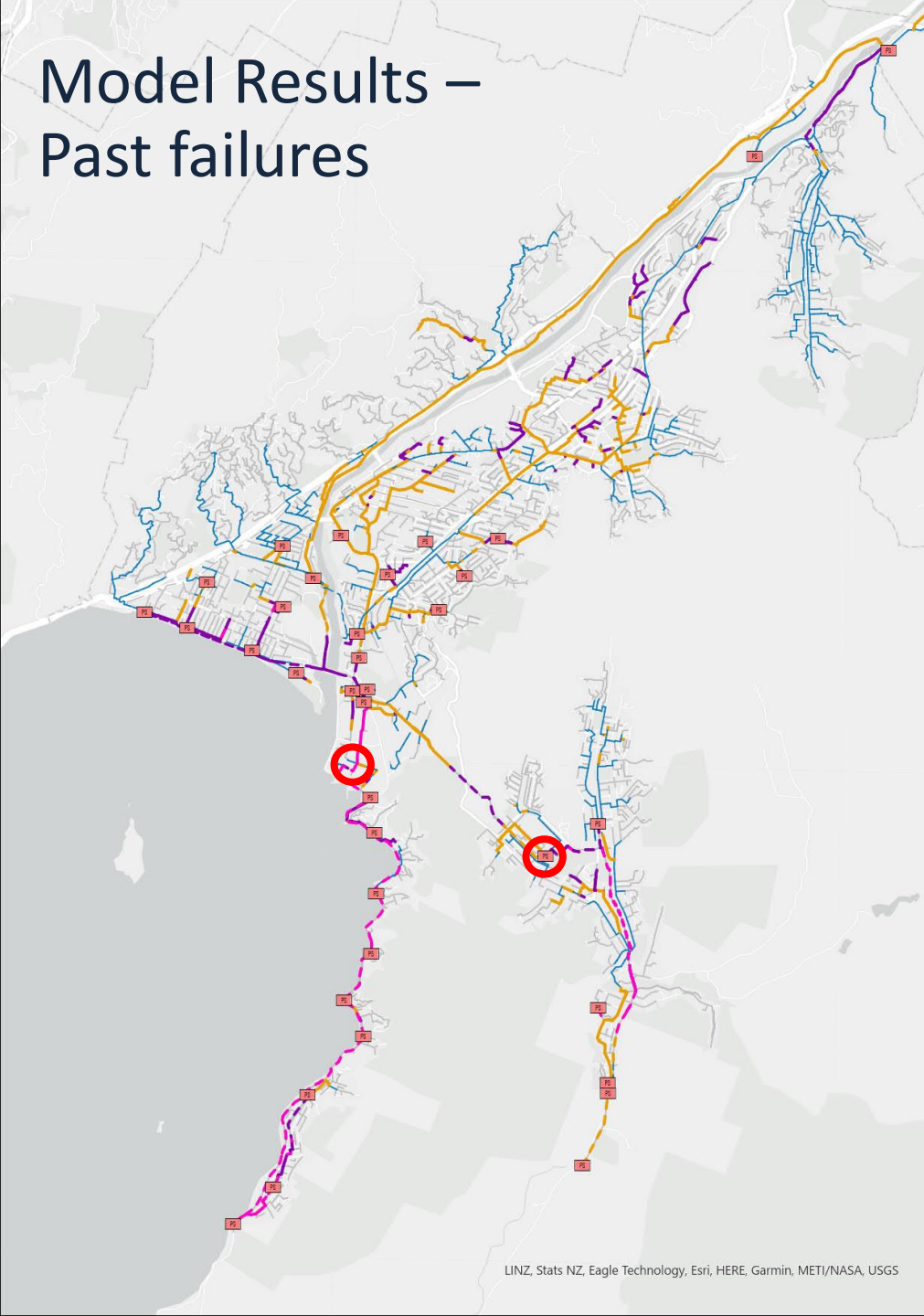
Model Results – Past failures



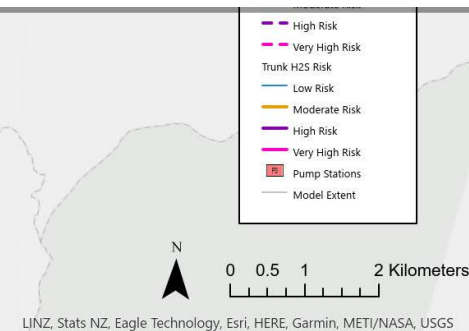
- Wise Park Wetwell after 10 years of receiving new RM
- Remedial epoxy coating and new drop structure with ventilation



Model Results – Past failures



- Collapsed – 2013, downstream of turbulent drop.
- 50m pipe replaced with HDPE.
- Ventilation pipe installed.





Future work

1. Other data collection to verify locations of concern
2. Inspection and monitoring programme
3. Modelling trial assessments in other networks (eg Moa Point)

Conclusions

1. ICM can estimate *dissolved* H_2S - an indicator of potential corrosion.
2. Dissolved H_2S is estimated using Pomeroy's Equation, which is inherently conservative.
3. For simplicity and stability, our trial case assumed constant temperature and pH – more conservative results.
4. Results can be filtered to prioritise RM discharge points and hydraulic jumps locations (~45 locations in Hutt Valley)
5. Due to the complexity and uncertainty involved, maps are presented as 'heat-maps' as a starting point for prioritising inspection locations.

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Questions

